



# The Vattenfall – Air Products Oxyfuel CO<sub>2</sub> Compression and Purification Pilot Plant at Schwarze Pumpe – Initial Results

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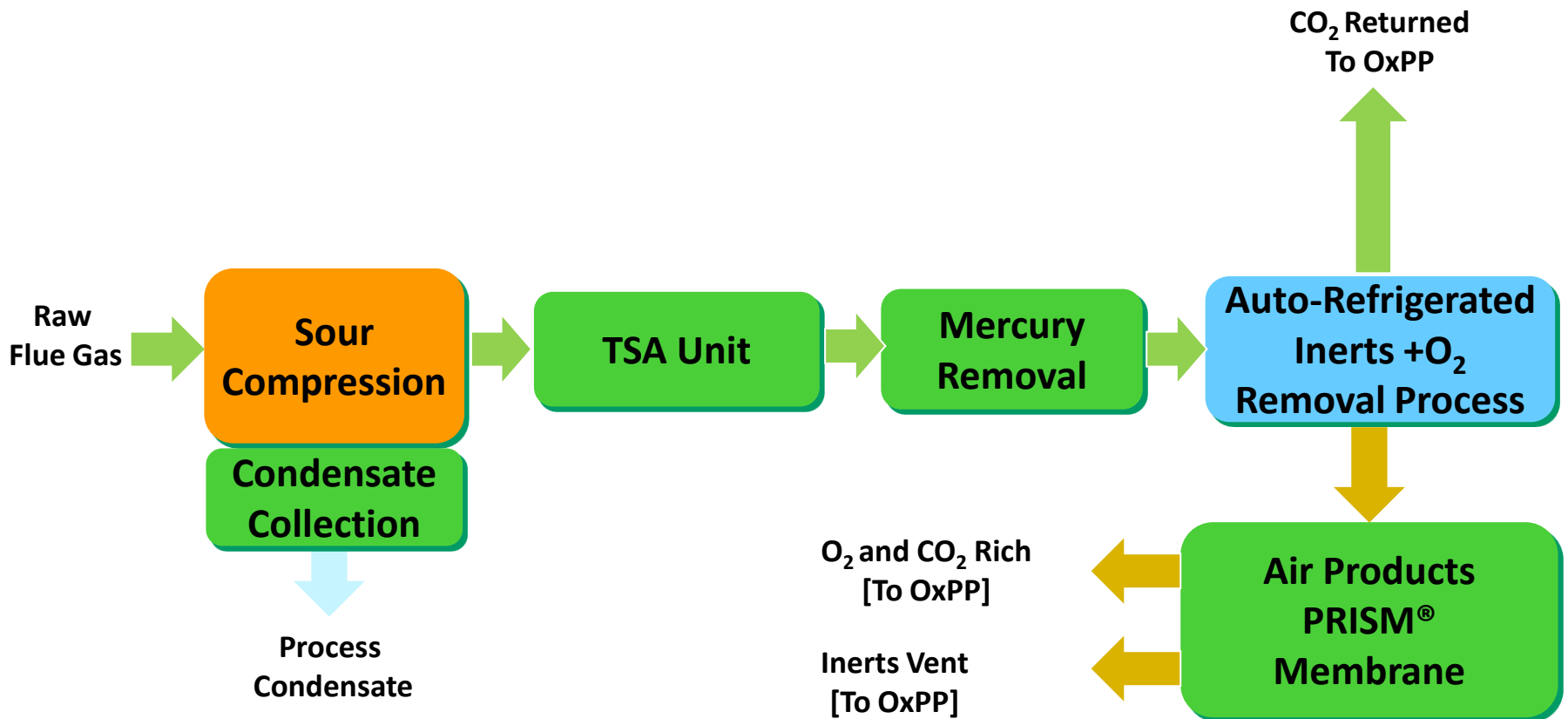
# The Vattenfall – Air Products Oxyfuel CPU Pilot Plant

- Review results from first few weeks of running
- Demonstrate how results show sour compression works
- Discuss the importance of understanding gas phase analysis and the effects of corrosion
- Share our experiences of running the auto-refrigerated inerts + O<sub>2</sub> removal process



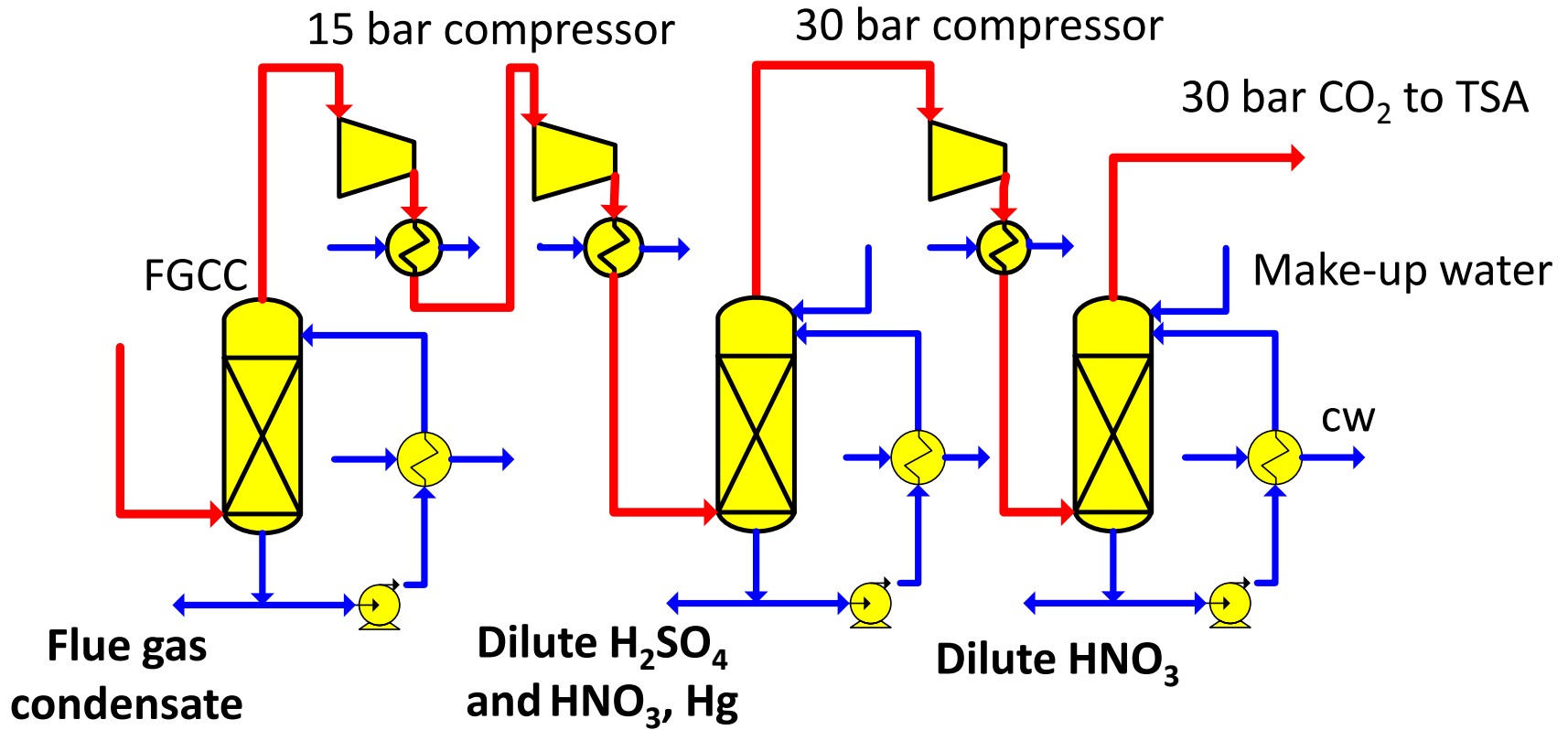


# Air Products' CO<sub>2</sub> Purification Unit (CPU) Pilot Plant at Vattenfall's Schwarze Pumpe OxPP





# Sour Compression: Removal of SO<sub>2</sub> & NO<sub>x</sub>





# Flue Gas Cooler Condenser

- Some SO<sub>2</sub> removal seen
- Only minor amounts of nitrates and nitrites found in the liquid phase
  - i.e. No NO<sub>x</sub> removal
- Removes all Chlorides (HCl) and all particulates



# Compression to 15 bar before 1<sup>st</sup> Column

- NO<sub>x</sub> only (No SO<sub>2</sub>)
  - NO<sub>x</sub> removal during compression
  - NO converted to NO<sub>2</sub>
- NO<sub>x</sub> and SO<sub>2</sub>
  - SO<sub>2</sub> removal during compression
  - Less NO<sub>2</sub> seen, confirming NO<sub>2</sub> that is formed reacts with SO<sub>2</sub> as expected





# Control of condensate formation during compression

- Need to control where condensate forms
- Temperature – Pressure – composition profile needs to be understood to prevent condensation, as acids will form
- First set of diaphragm compressor valves incorrectly specified with incompatible material
  - Mode of operation caused condensation, hence acid formation
  - Not all stainless steels are equal!



**And what happens when the correct valve material is selected:**



# 15 bar column

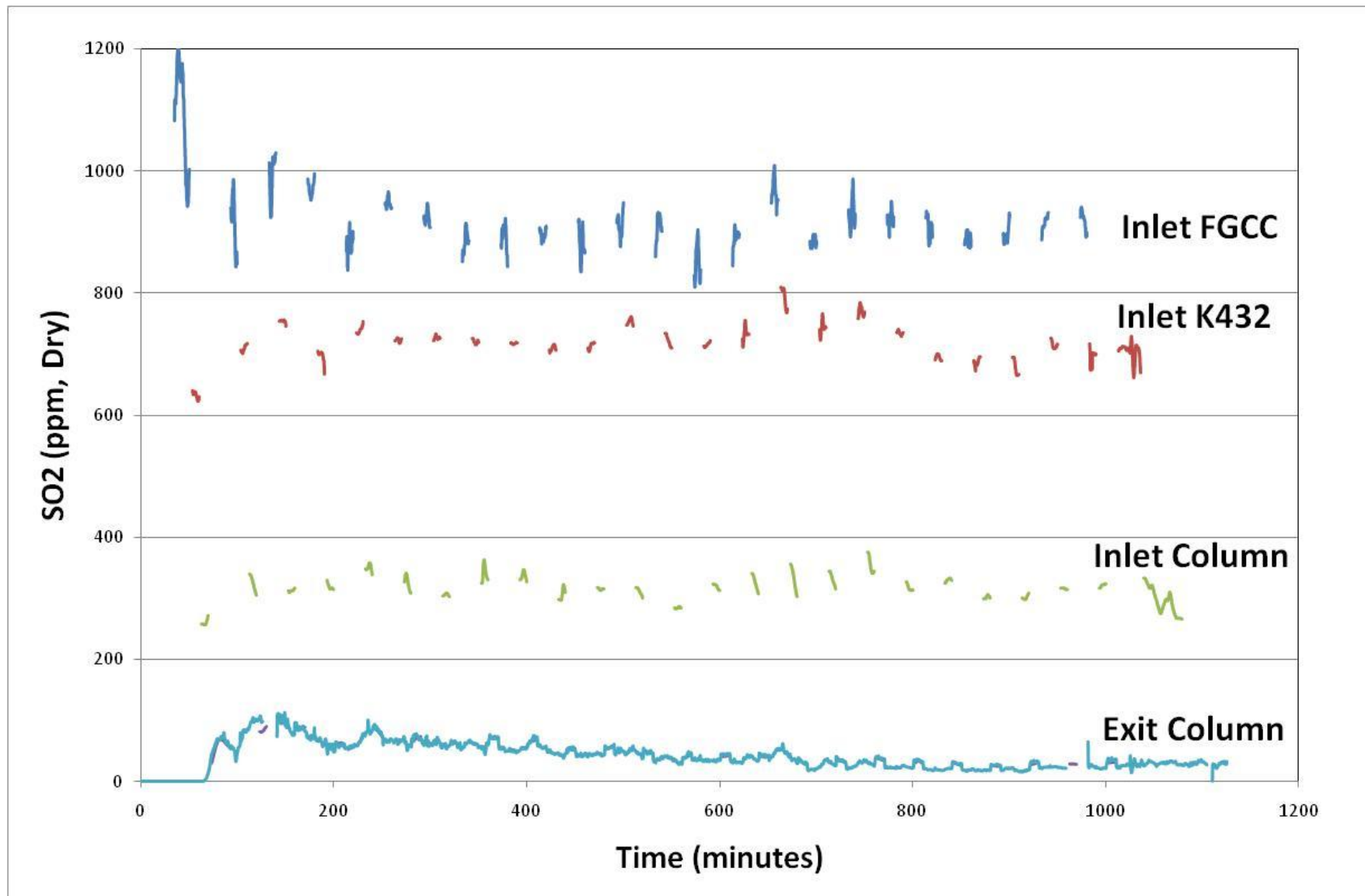
- NOx only (No SO<sub>2</sub>)
  - Almost complete NOx removal – 30 bar column polished off the rest
- NOx and intermediate levels of SO<sub>2</sub>, taken from up and downstream FGD
  - ~90% NOx removal
  - ~90% SOx removal
- NOx and high levels of SO<sub>2</sub>, taken from upstream of the FGD
  - Only preliminary results at the moment at 2500 ppm SO<sub>2</sub> (dry) from a short test just before shutting down for the OxPP burner changeout
  - Results are very encouraging but need verifying when the plant restarts
  - Will be presented when we have more data





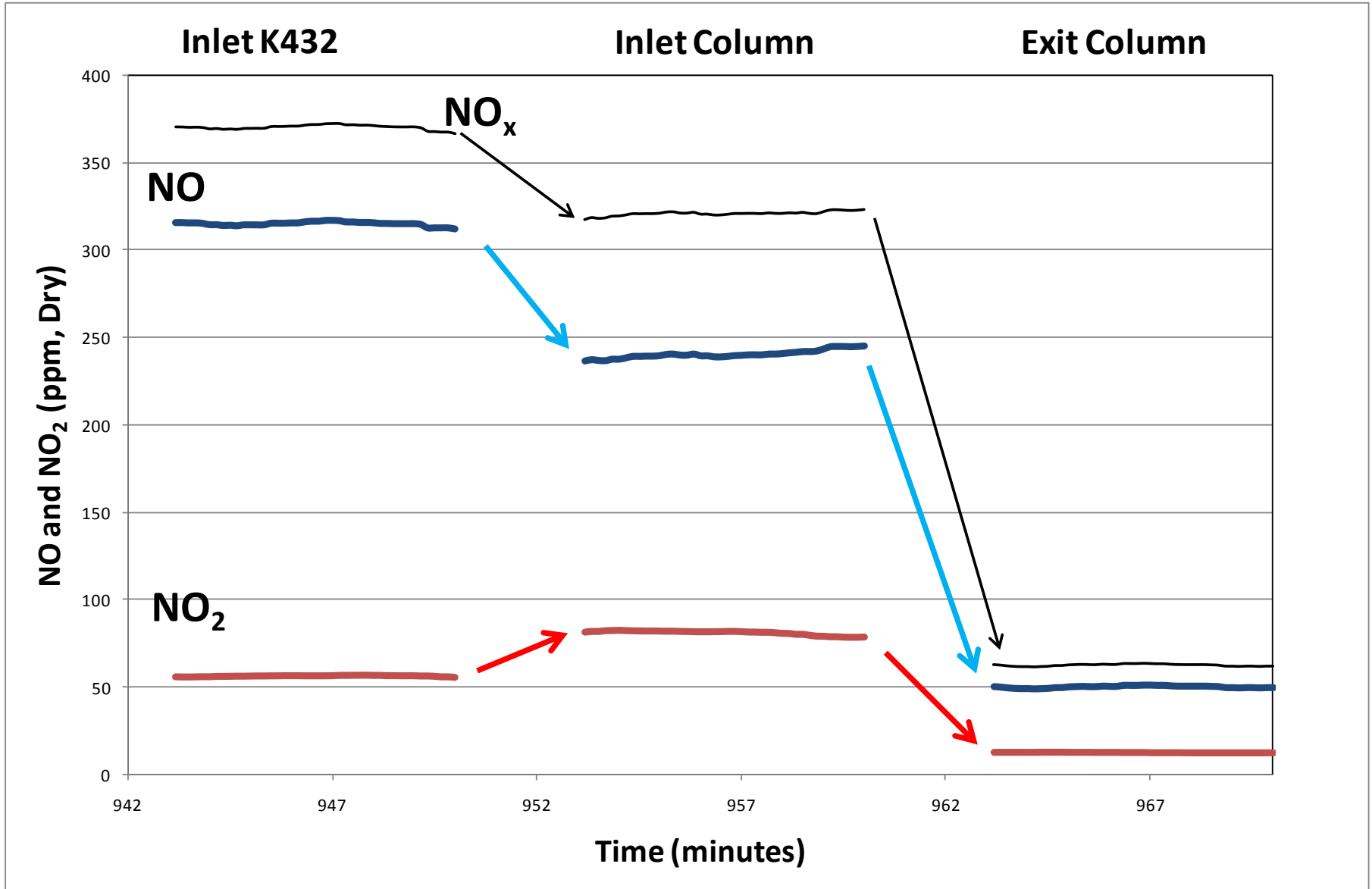


# 50/50 Flue Gas Mix From Before and After OxPP FGD





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# Liquid and Gas Phase Analysis

- Liquid analysis for nitrate/ite, sulphate/ite
- SO<sub>2</sub>, NO, NO<sub>2</sub> analysis of wet flue gas streams is difficult
  - ACPP and OxPP both using new type of analyser from SICK Maihak
    - Calibration is complex and unique to each analyser
    - Multi-dimensional calibration curve to compensate for NO<sub>2</sub>, H<sub>2</sub>O, CO<sub>2</sub> (etc) cross interference
  - Results cross-checked with Teledyne and Rosemount analysers where possible
- Very easy to believe analysers – more difficult to cross check and verify
  - But critical to the success of this project
- Also seen N<sub>2</sub>O in certain conditions
  - Need more work to understand N<sub>2</sub>O formation



# Corrosion Coupon Racks

- To help understand materials of construction and the effects of the acids on these materials, corrosion coupon racks were used
- Most coupons just as “shiny” as they were when they were new
- However, as expected, we have seen attack on corrosion coupons that are in the chloride containing part of the system.
  - which is why we have made the dirty end of the FGCC out of fibreglass.





# Auto-refrigerated Inerts removal process

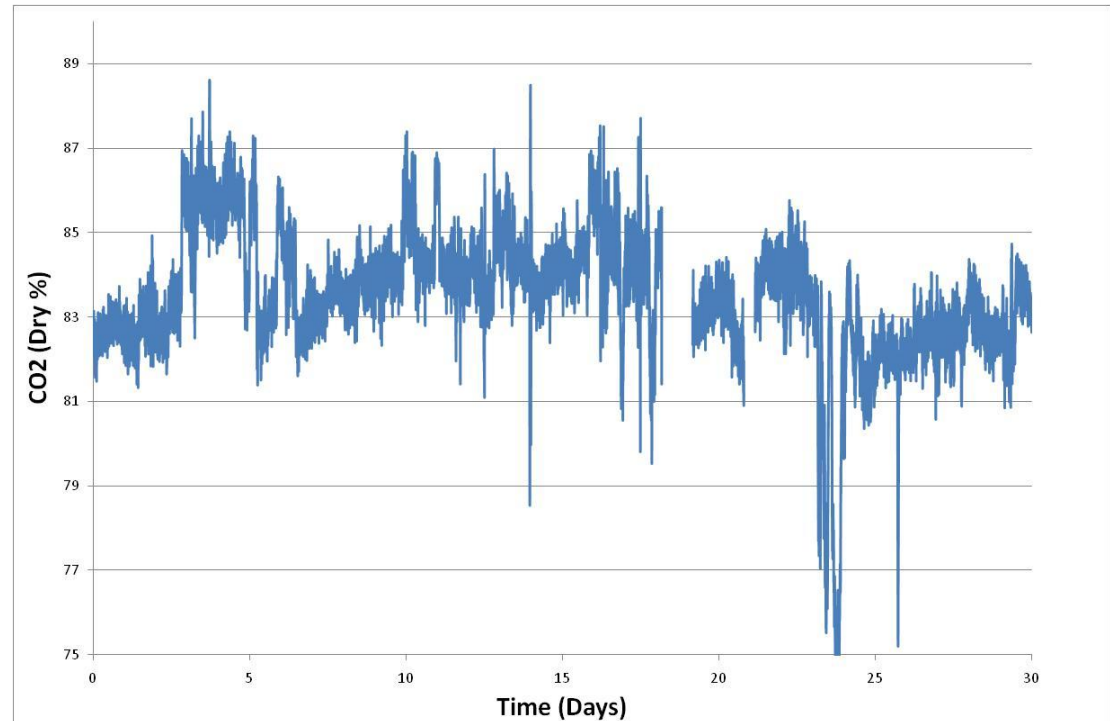
- This is the cold end of the system including the heat exchanger and distillation stripping column
  - Removes  $N_2/Ar/O_2$  from the  $CO_2$
  - Optional distillation column for high purity  $CO_2$
- Process is auto-refrigerated – an integrated, efficient process that uses the  $CO_2$  product as the refrigerant





# Feed composition variation

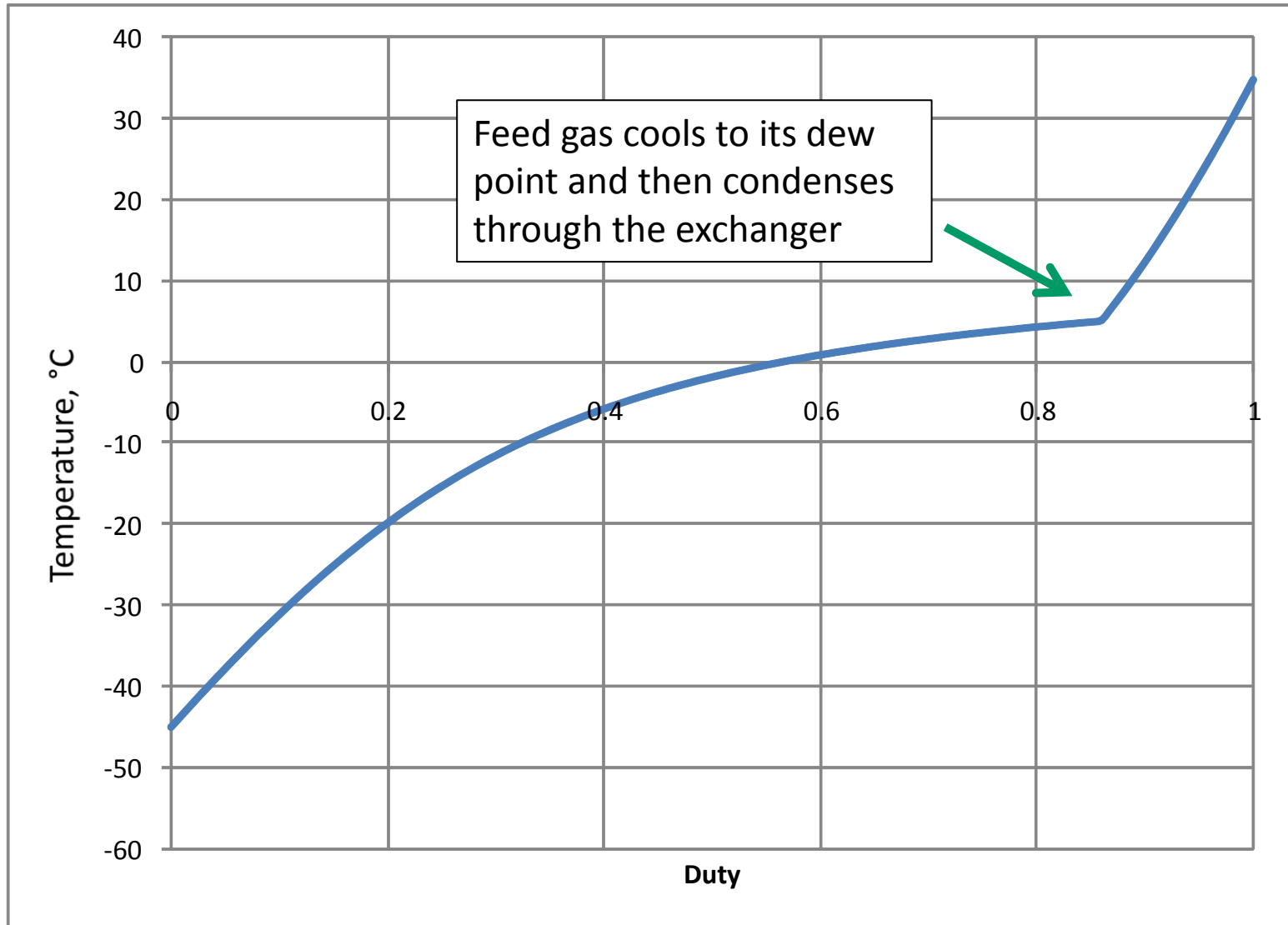
- Variations in flue gas composition from the OxPP
  - Normally 81-87% CO<sub>2</sub>
  - But spikes to 89% and drops to 75%
- This variation affects the performance of the inerts removal process
- Understanding the effect on the heat exchanger cooling curve will allow better control, for better performance and higher CO<sub>2</sub> recovery





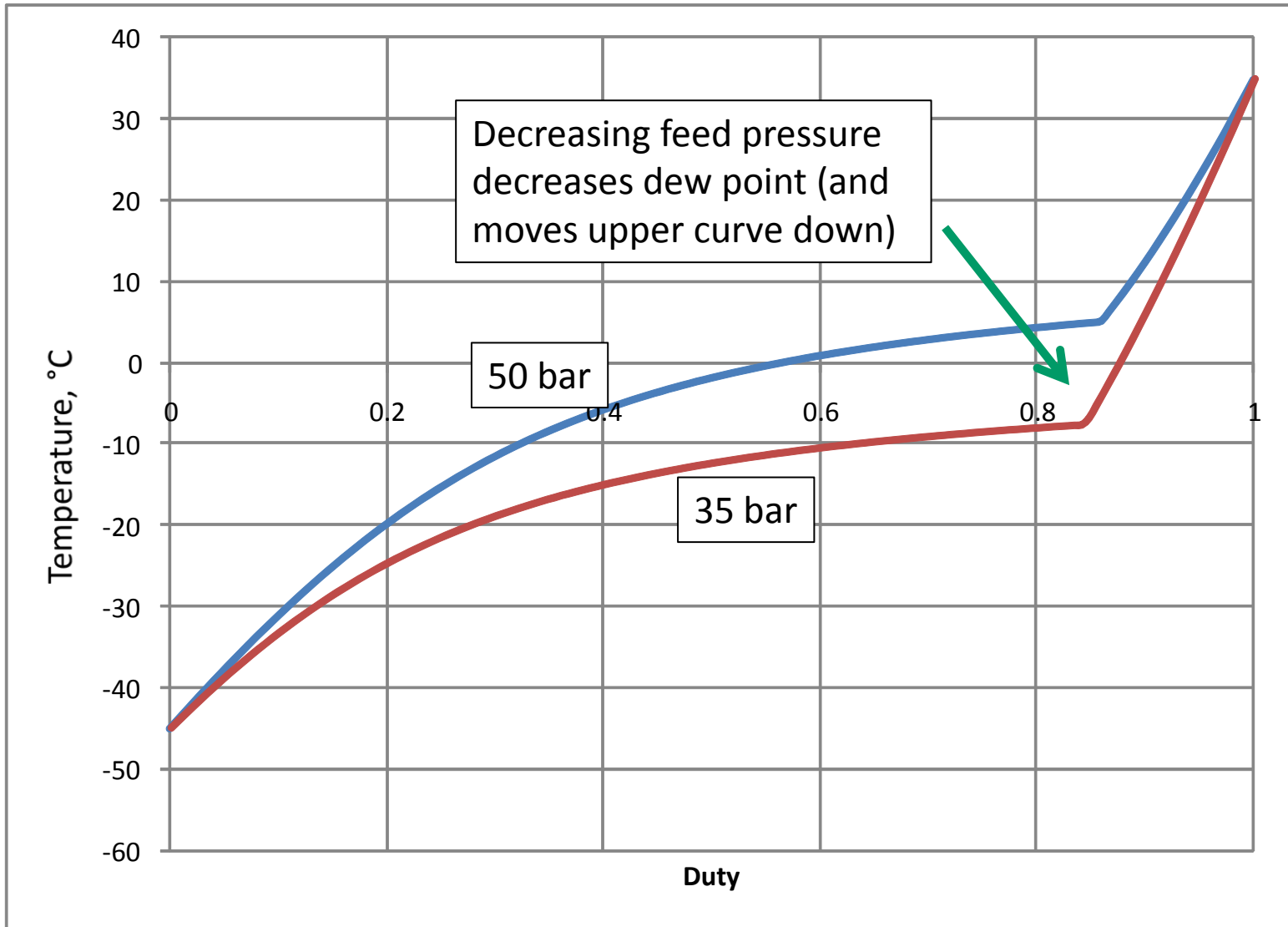


# Cooling Curve Low Purity Mode



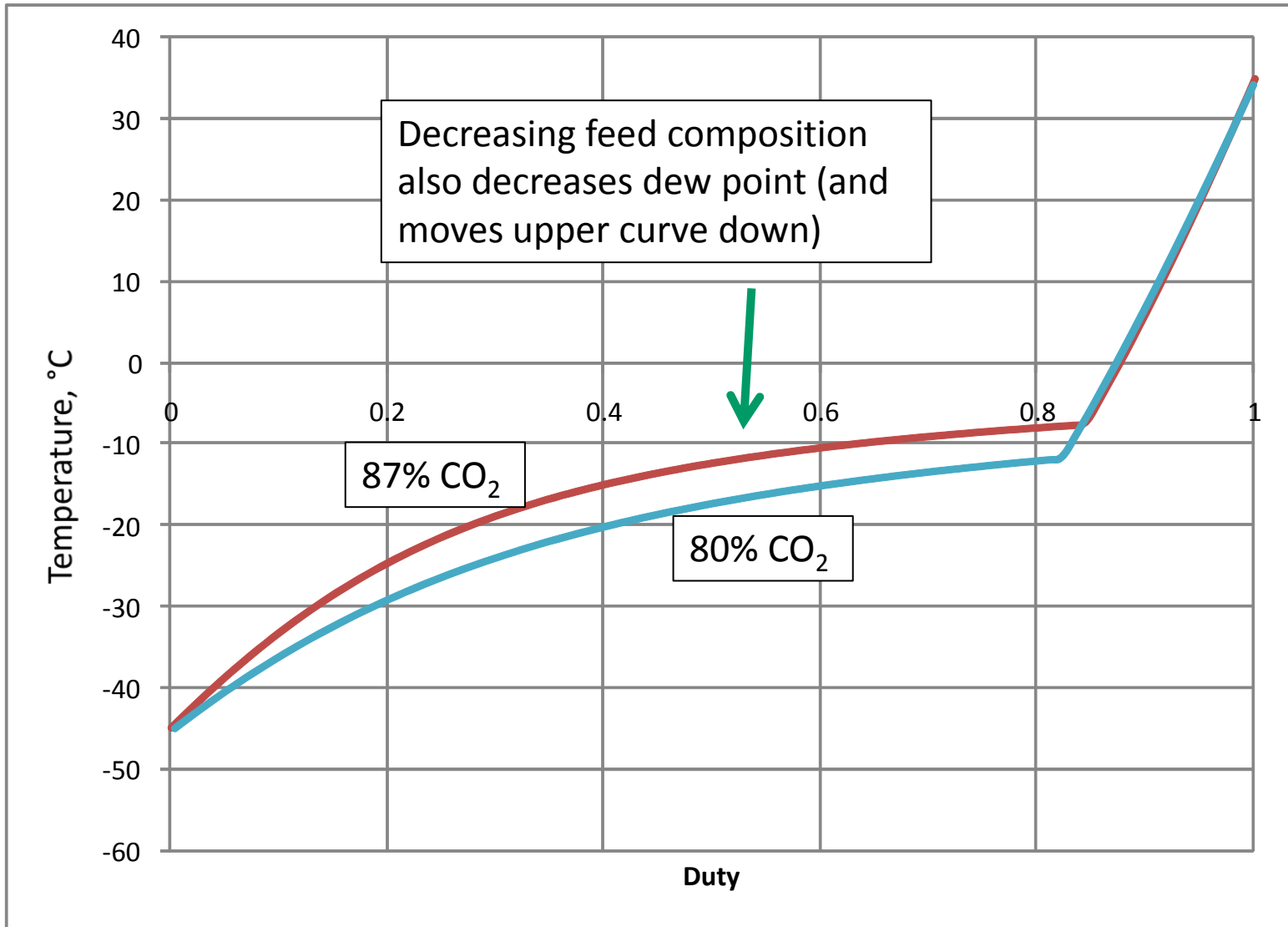


# Cooling Curve Low Purity Mode





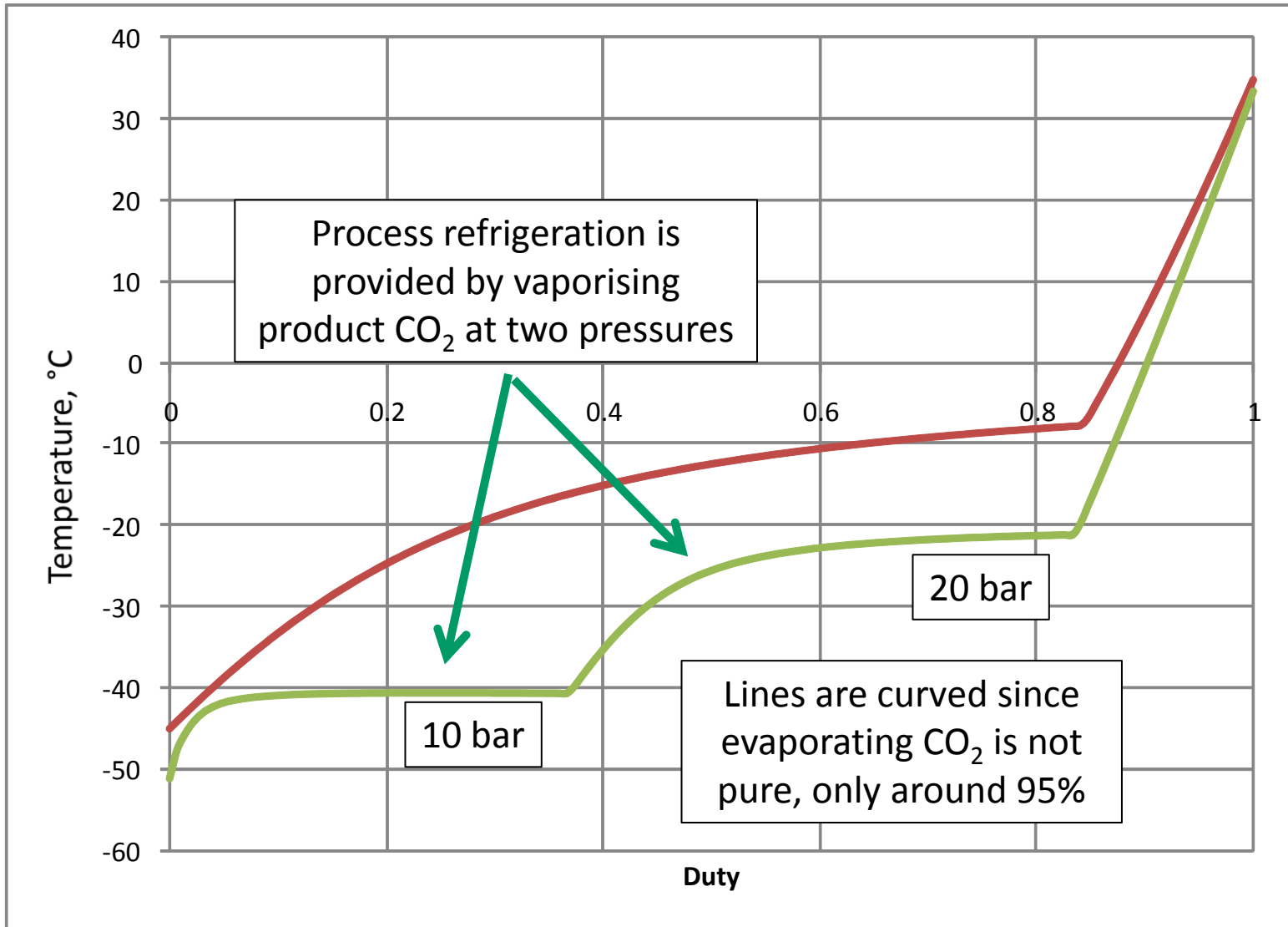
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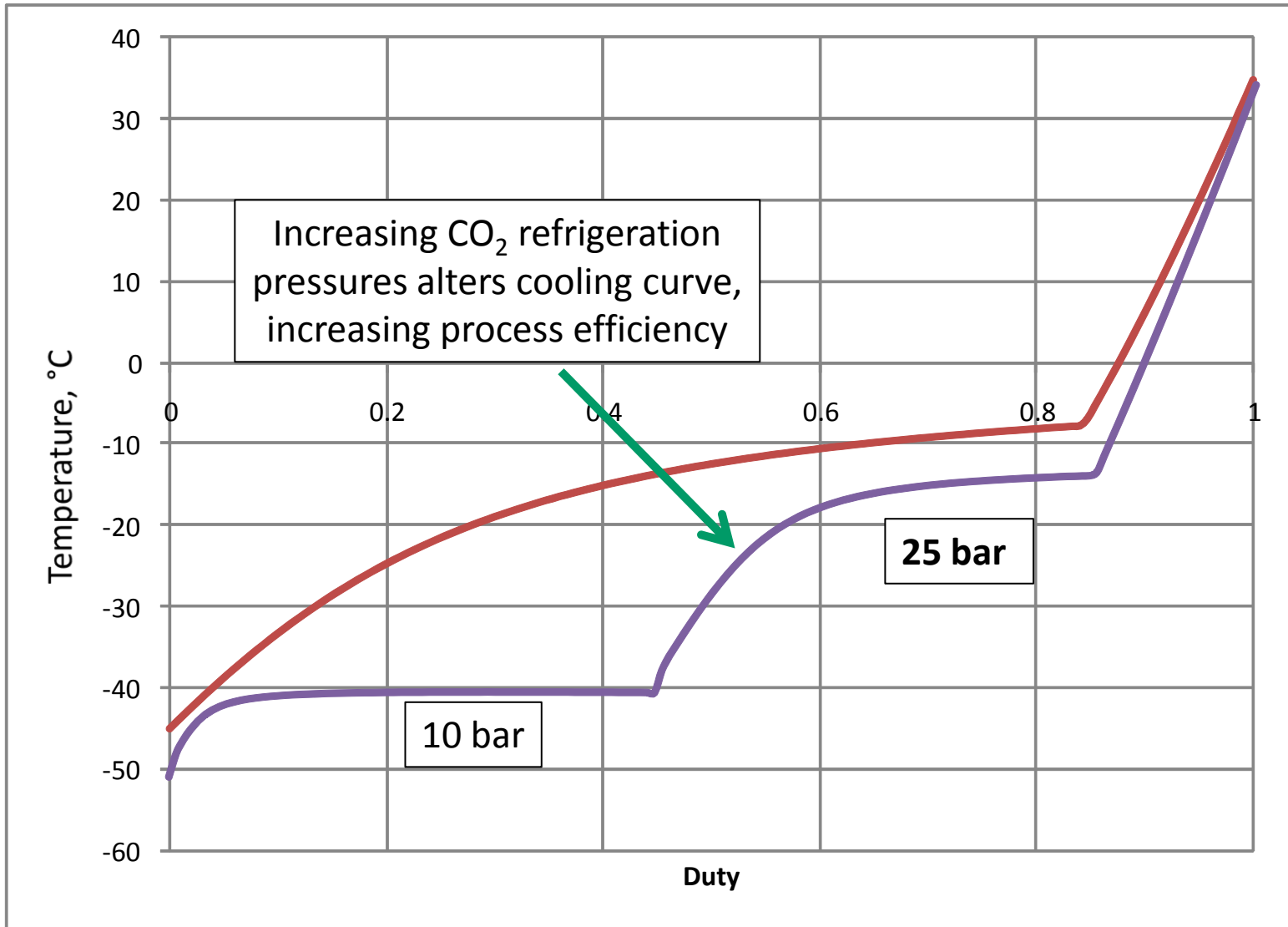


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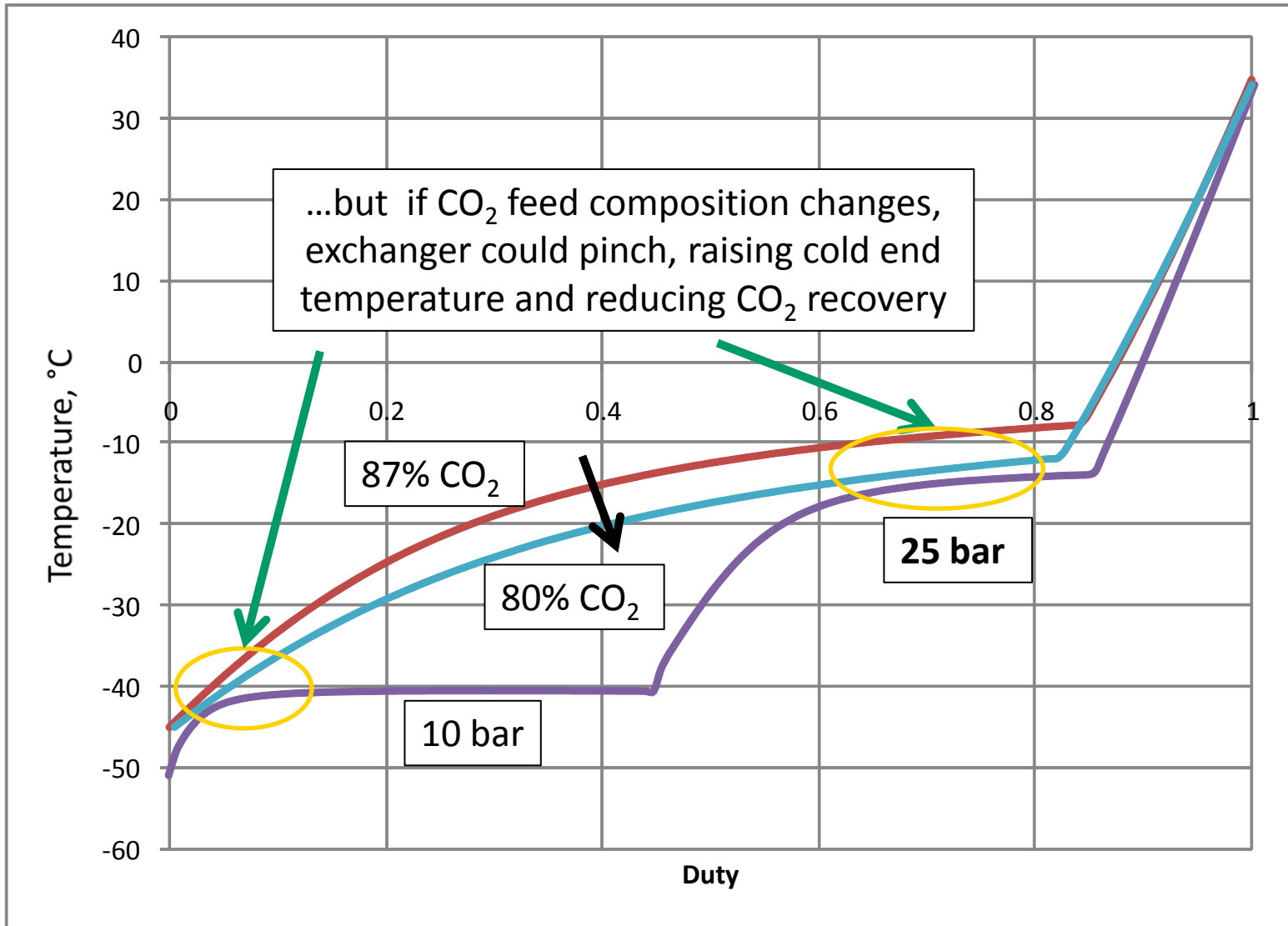


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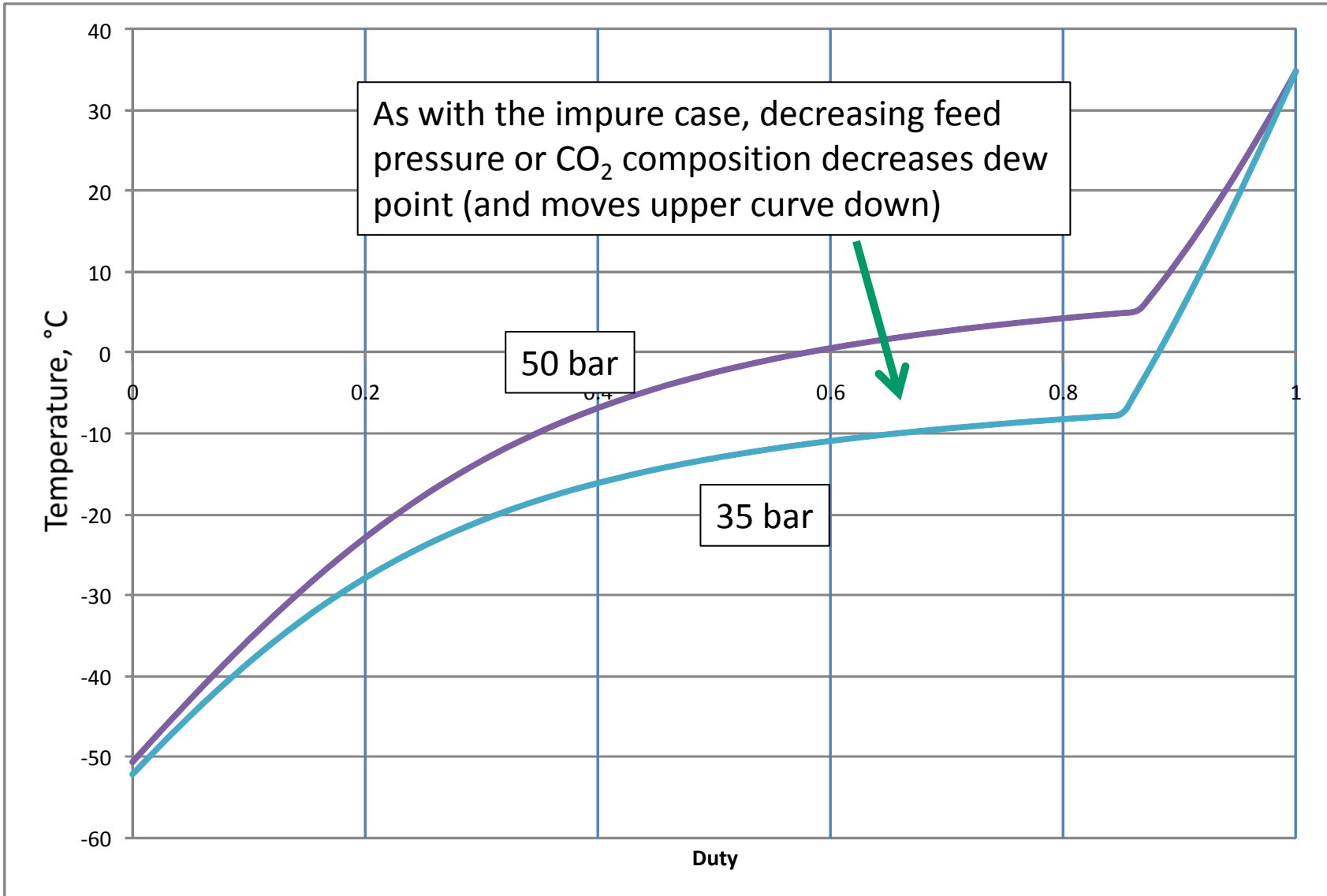


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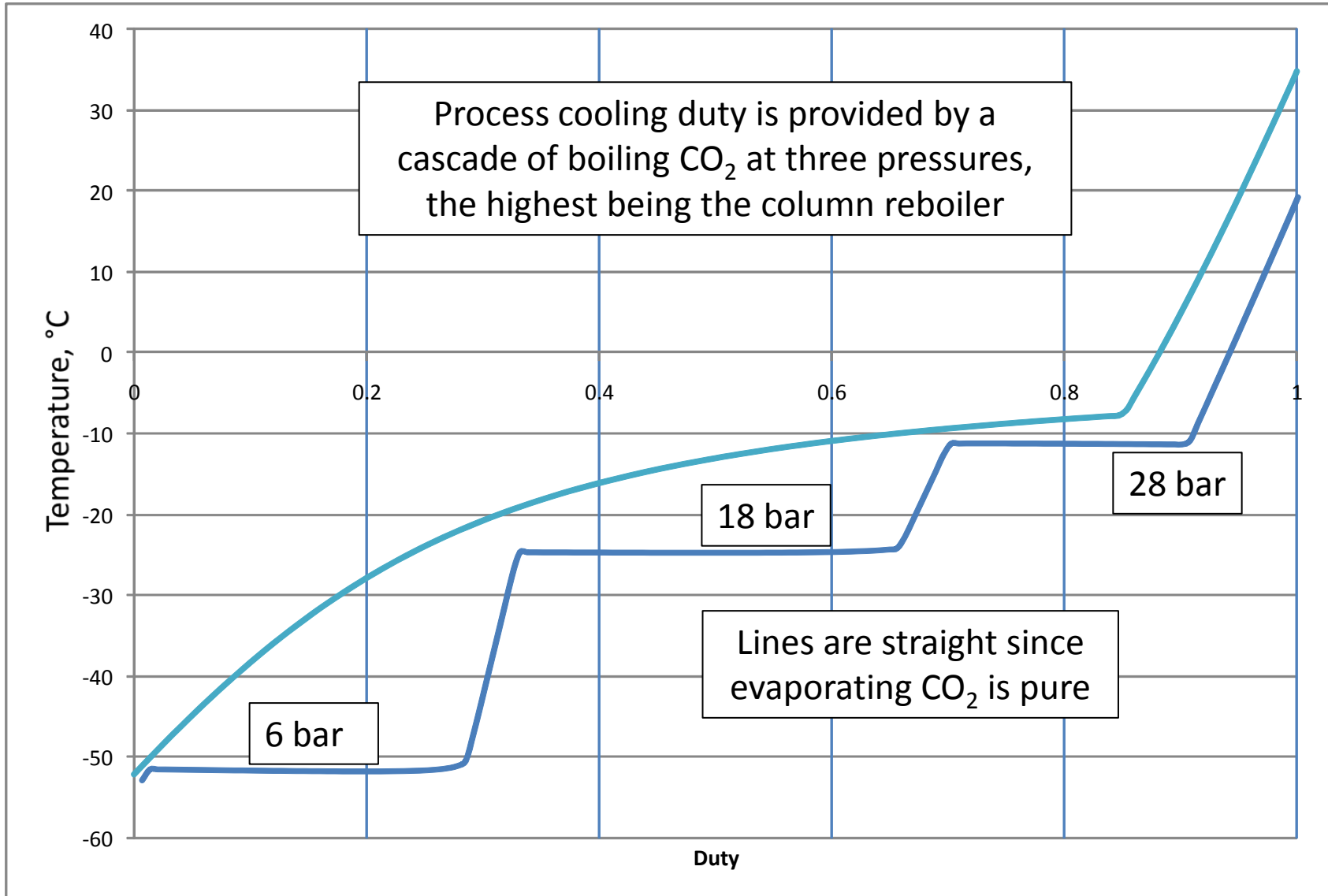


# Cooling Curve – Pure CO<sub>2</sub>



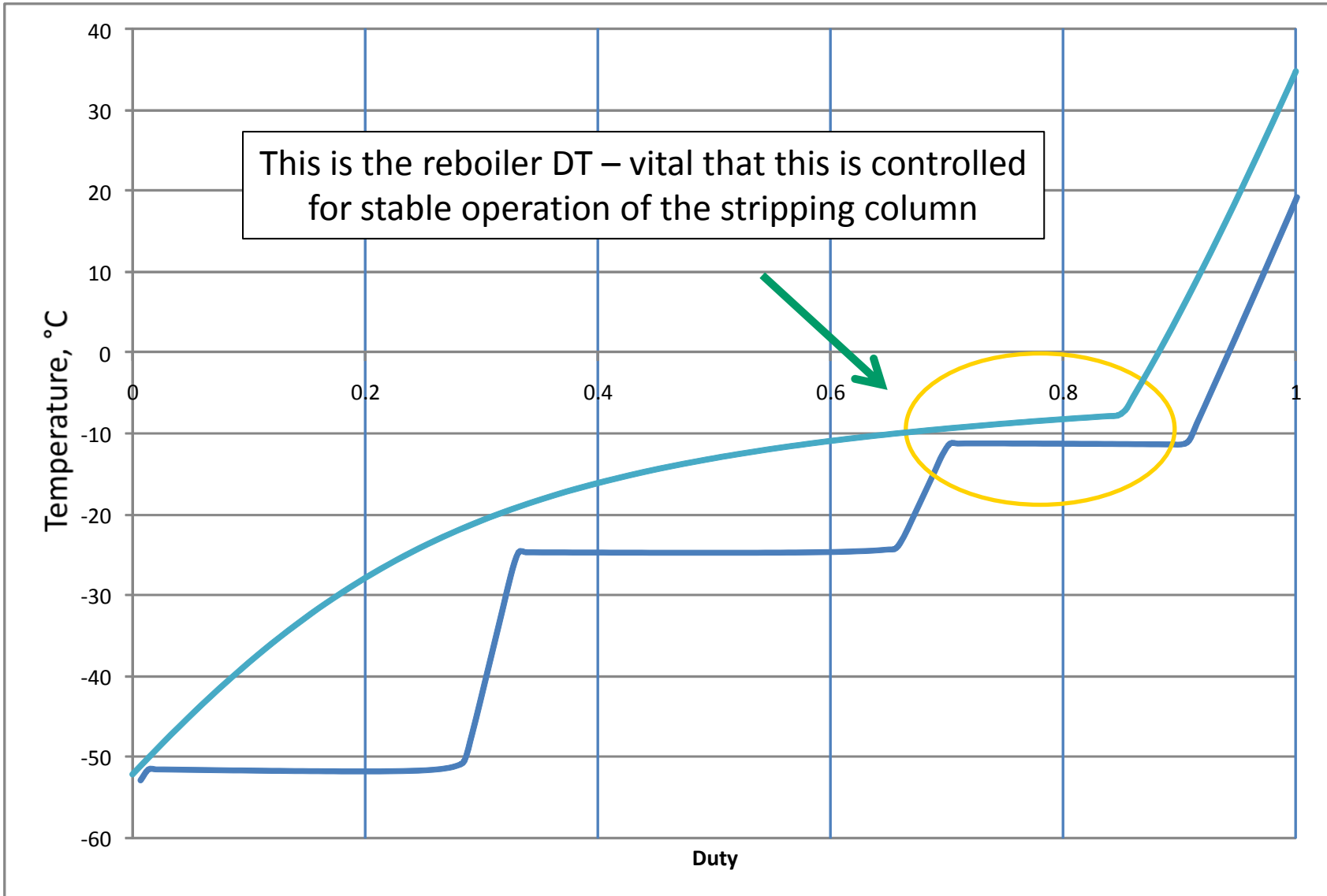


# Cooling Curve – Pure CO<sub>2</sub>



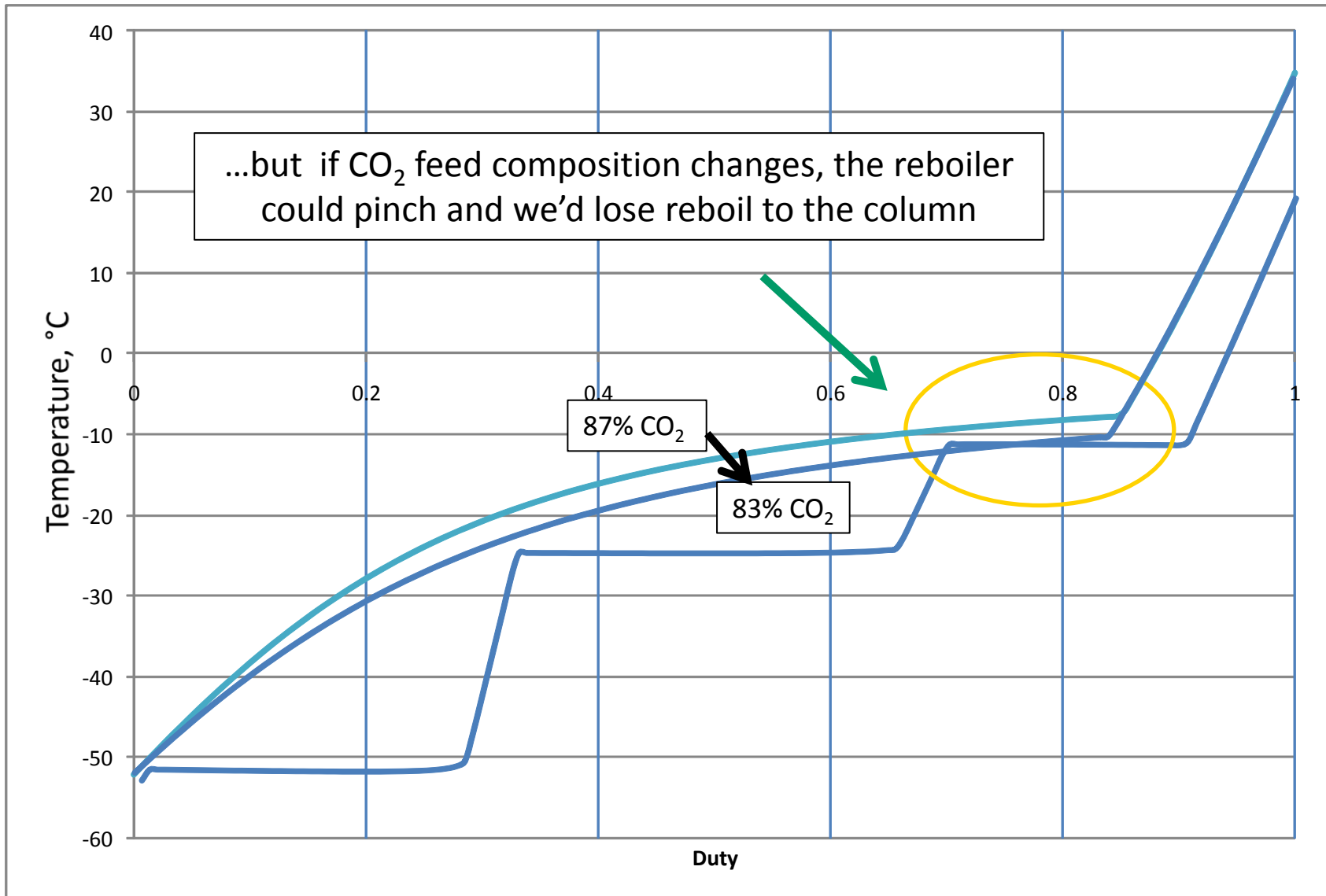


# Cooling Curve – Pure CO<sub>2</sub>





# Cooling Curve – Pure CO<sub>2</sub>





# Operation of the inerts removal system

- Disturbances from feed composition variation need to be expected and mitigated
- Feed cooling curve can be influenced by the condensing pressure
- LP CO<sub>2</sub>, MP CO<sub>2</sub> and reboiler pressures control heat exchanger performance
- Pressures need to be controlled to maintain the exchanger temperature profile
- Reboiler DT needs particular attention – can't be too wide nor too narrow
- Solution we are adopting is to feed forward the operating pressures from the feed CO<sub>2</sub> composition





# Compromises made for the pilot plant

- We do pilot plants to learn and make compromises in the design for many reason, particularly due to the small size of the plant
  - Not practical to use the same equipment that would be used in a full scale plant
- Compressors
  - Due to the required flowrate we couldn't use the turbo-machinery that would be used on demonstration plants
  - Needed to avoid machinery that would affect the sour compression chemistry, such as water-flooded screw compressors
  - Selected diaphragm compressors – not ideal for this application but chosen because of the flow range required
- Inerts removal system
  - To simplify the system a cycle was chosen that included feed compression
  - Reboiler integrated into the main exchanger
  - Small size of equipment increases the effect of heat leak





# Conclusions

- **First demonstration of Sour Compression in representative equipment**
  - Although only limited running so far, results are very encouraging and support the Sour Compression theory
- **First demonstration of auto-refrigerated inerts removal**
  - Running of the inerts removal process challenging due to the variation of the feed composition and its affect on the heat exchanger cooling curve
  - Understanding this behaviour now means we can set the control system to respond correctly
- **Learned many lesson relevant to full scale plant design and operation**
  - Operation under realistic conditions
  - Materials of construction
  - Analysis of wet flue gas
- **Testing to restart in the Autumn, once OxPP restarts with new burner**





Thank you

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