

Development and application of a novel radiation property model for oxy-coal combustion

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- ❑ Background
- ❑ The Full Spectrum k-Distributions (FSCK) model
- ❑ Application
 - Doosan Babcock Clean Coal Test Facility (CCTF)
 - Results
- ❑ Conclusions and way forward



- High temperatures in coal combustion mean that radiation dominates the heat transfer
- Numerical solution of the **radiative transfer equation (RTE)**

$$\begin{array}{|c|} \hline \text{Change in intensity} \\ \text{over a pathlength } ds \\ \text{in elementary solid} \\ \text{angle} \\ \hline \end{array} = \begin{array}{|c|} \hline \text{Emission} \\ \hline \end{array} - \begin{array}{|c|} \hline \text{Absorption and} \\ \text{out scattering} \\ \hline \end{array} + \begin{array}{|c|} \hline \text{In scattering of intensity} \\ \text{from all other directions} \\ \hline \end{array}$$

- Radiative property model needed

$$\begin{array}{|c|} \hline \text{Air-fuel combustion} \\ \text{environment} \\ \hline \end{array} \neq \begin{array}{|c|} \hline \text{Oxy-fuel combustion} \\ \text{environment} \\ \hline \end{array}$$



Line-by-line

$[d\eta < 2\text{cm}^{-1}, N > 10^6]$

Narrow-band models

- Statistical narrow band
- Correlated-k

$[d\eta \approx 25\text{cm}^{-1}, N > 300]$

$[d\eta > 50\text{cm}^{-1}, N > 300]$

Wide-band models

- Exponential wide-band model

$[d\eta \approx 1000\text{cm}^{-1}, N > 7]$

Global models

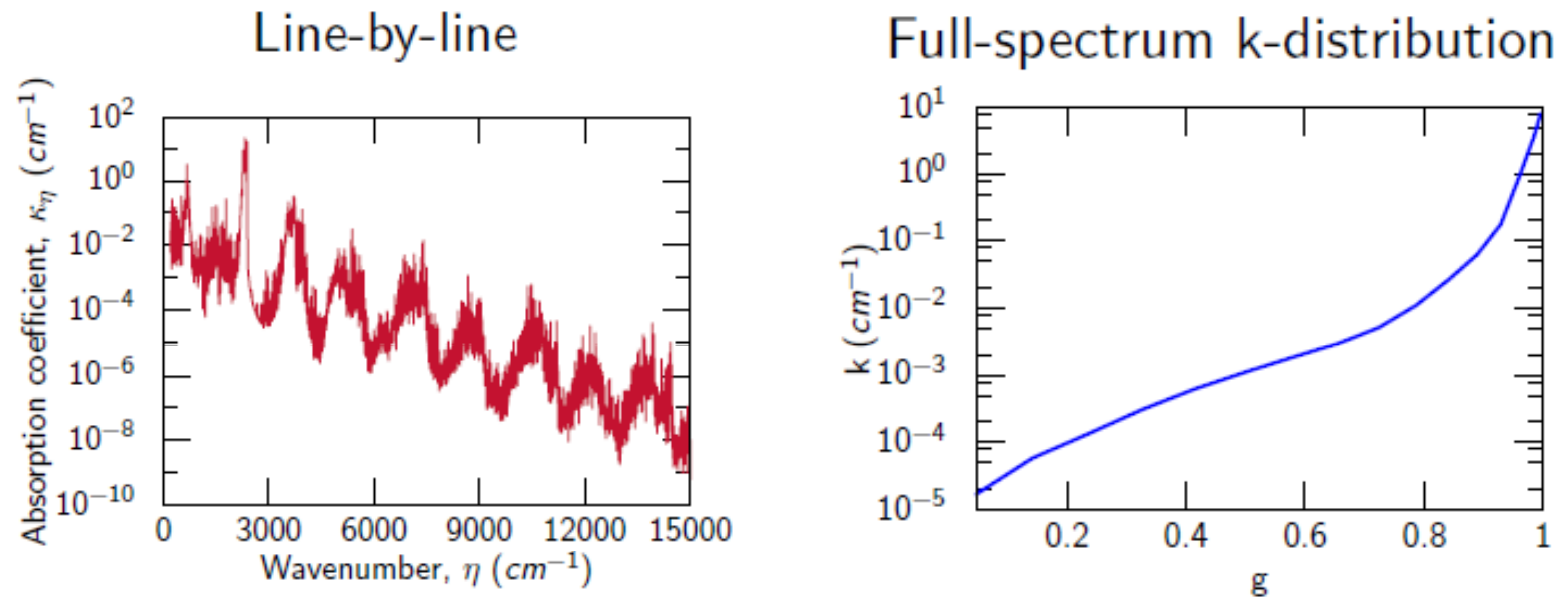
- Weighted sum of grey gases
- Grey weighted sum of grey gases
- Full-spectrum k-distribution

$[N > 3]$

$[N = 1]$

$[N > 4]$

Simplify spectral integration of intensity by rearranging κ_n



85% CO_2 , 10% H_2O , 5% N_2 mixture at 1000K

Models first proposed by Modest and Zhang (2002)

The RTE for the FSCK method:

$$\frac{dI_\eta}{d\hat{s}} = \kappa_\eta I_{b\eta}(T) - \kappa_\eta I_\eta - \sigma_{s\eta} I_\eta + \frac{\sigma_{s\eta}}{4\pi} \int_{4\pi} I_\eta(\hat{s}') \Phi(\eta, \hat{s} \cdot \hat{s}') d\Omega$$



$$\frac{dI_g}{d\hat{s}} = k^*(T_0, \underline{\phi}, g_0) \left(a(T_0, T, g_0) I_b(T) - I_g \right) - \sigma_s I_g + \frac{\sigma_s}{4\pi} \int_{4\pi} I_g(\hat{s}') \Phi(\hat{s} \cdot \hat{s}') d\Omega$$

Integration can be done through a Gauss-quadrature scheme

$$\int_0^\infty I_\eta d\eta = \int_0^1 I_g dg_0 \approx \sum_{i=1}^{N_q} w(i) I_{gi}$$

Previously demonstrated in CFD by Porter et al. (2010)



Effective particle radiation:

$$\kappa_P = \frac{1}{V} \sum_P Q_{abs} \pi r^2$$

$$E_{P,g} = \frac{1}{V} \sum_P Q_{abs,P} \pi r_P^2 a(T_0, T_P, g_0) I_b(T_P)$$

$$\sigma_{S,P} = \frac{1}{V} \sum_P Q_{sca} \pi r^2$$

The RTE for the FSCK method with particles:

$$\frac{dI_g}{d\hat{s}} = k^*(T_0, \underline{\phi}, g_0) \left(a(T_0, T, g_0) I_b(T) - I_g \right) + E_{P,g} - \kappa_P I_g - (\sigma_s + \sigma_{S,P}) I_g + \frac{(\sigma_s + \sigma_{S,P})}{4\pi} \int_{4\pi} I_g(\hat{s}') \Phi(\hat{s} \cdot \hat{s}') d\Omega$$



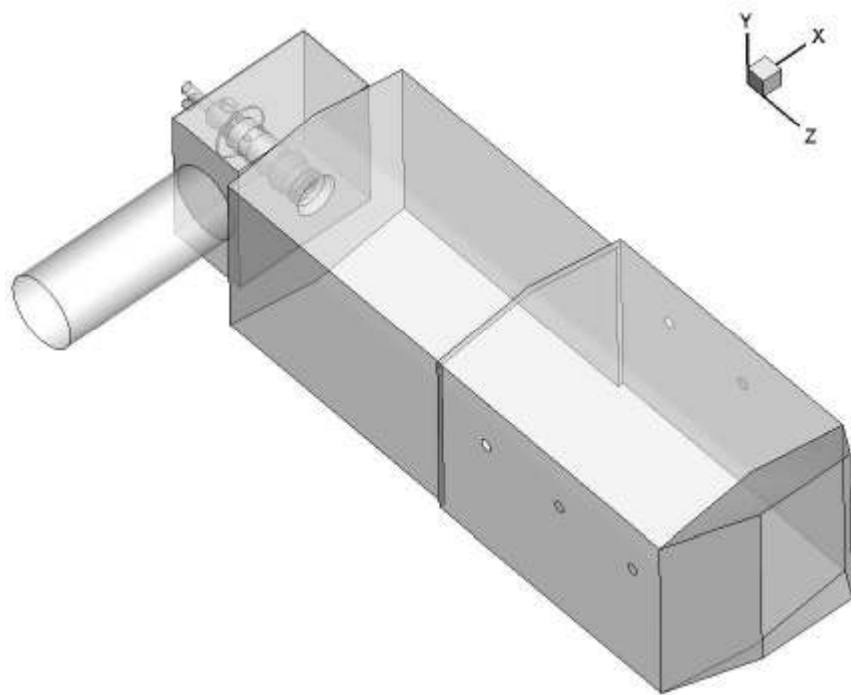
Gas Radiation

- Directional radiation transfer by the DO method
- Solid angle discretisation $N_{\theta} = N_{\phi} = 3$
- Radiation included from CO₂, H₂O and CO
- Mixing scheme from Modest and Riazzi (2005)
- k-distributions calculated from NB k-g database

Particle Radiation

- Particle absorption efficiency $Q_{\text{abs}} = 0.9$
- Particle scattering efficiency $Q_{\text{sca}} = 0.01$
- Isometric scattering phase function

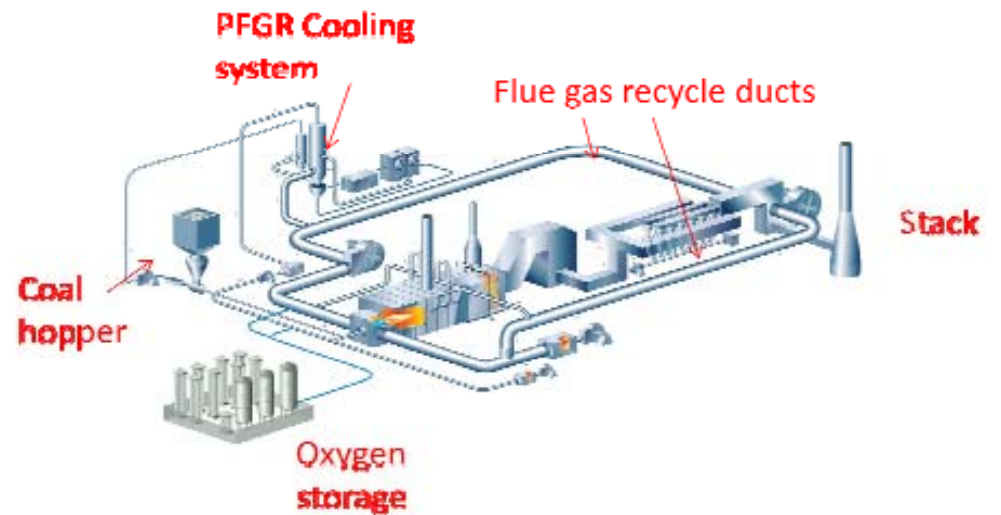
Doosan Babcock Clean Coal Test Facility (CCTF)



40MW_{th}

Air- and oxy-coal combustion

Single, low NO_x burner



Test conditions



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Operating Conditions		
Burner zone stoichiometry		1.0
FGR rate %		60.0
Mass flow (kg/s)	Windbox	8.61
	Primary	3.32
	Core	0.4
	Total	12.33
Coal flow rate (kg/s)		1.18
O ₂ in primary		19.7
O ₂ in windbox		30.0
CO ₂ in primary		63.04
CO ₂ in windbox		50.88
H ₂ O in windbox		7.41

Coal analysis (%) El Cerrejon	
HCV as r.	3.159e+7 MJ/kg
Ash	2.3
Moisture	2.9
FC	58.5
VM	36.3
C	77.90
H	5.06
N	1.68
S	0.68
Cl	0.02
O	9.49



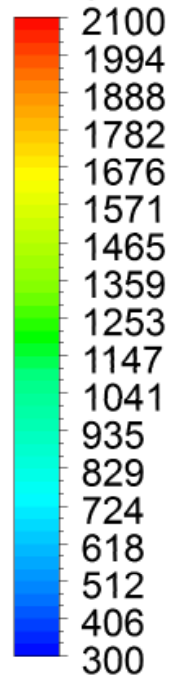
- CFD simulation using ANSYS Fluent v12.1
- RANS, full 3D model, 4M cells
- Turbulence-chemistry interaction: eddy dissipation
- Two-step global reaction for volatile combustion
- Devolatilisation: single rate
($A_0 = 14841 \text{ s}^{-1}$; $E_a = 35.3 \text{ MJ/kmol}$)
- Char combustion: intrinsic model
($A_0 = 4.0\text{e-}04 \text{ kg/m}^2\text{-s-Pa}$; $E_a = 66 \text{ MJ/kmol}$)

Results

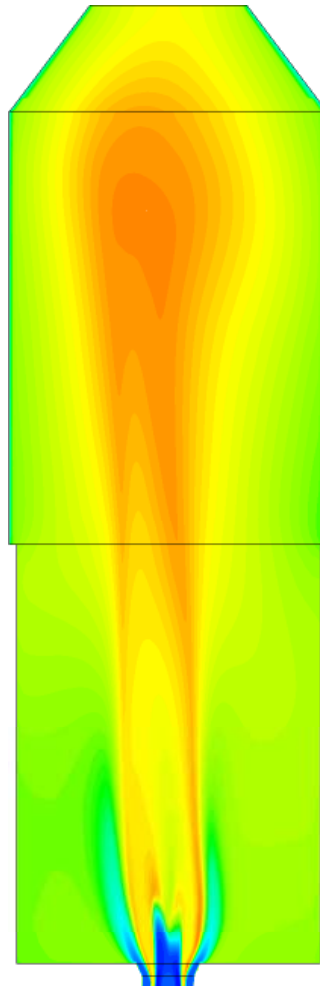


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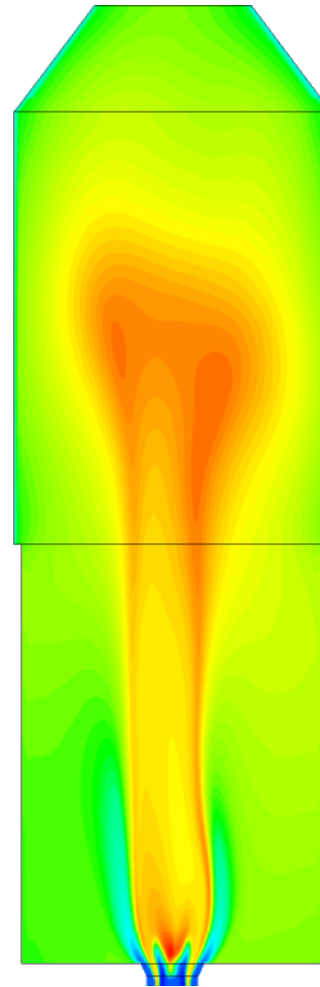
Temperature



[K]



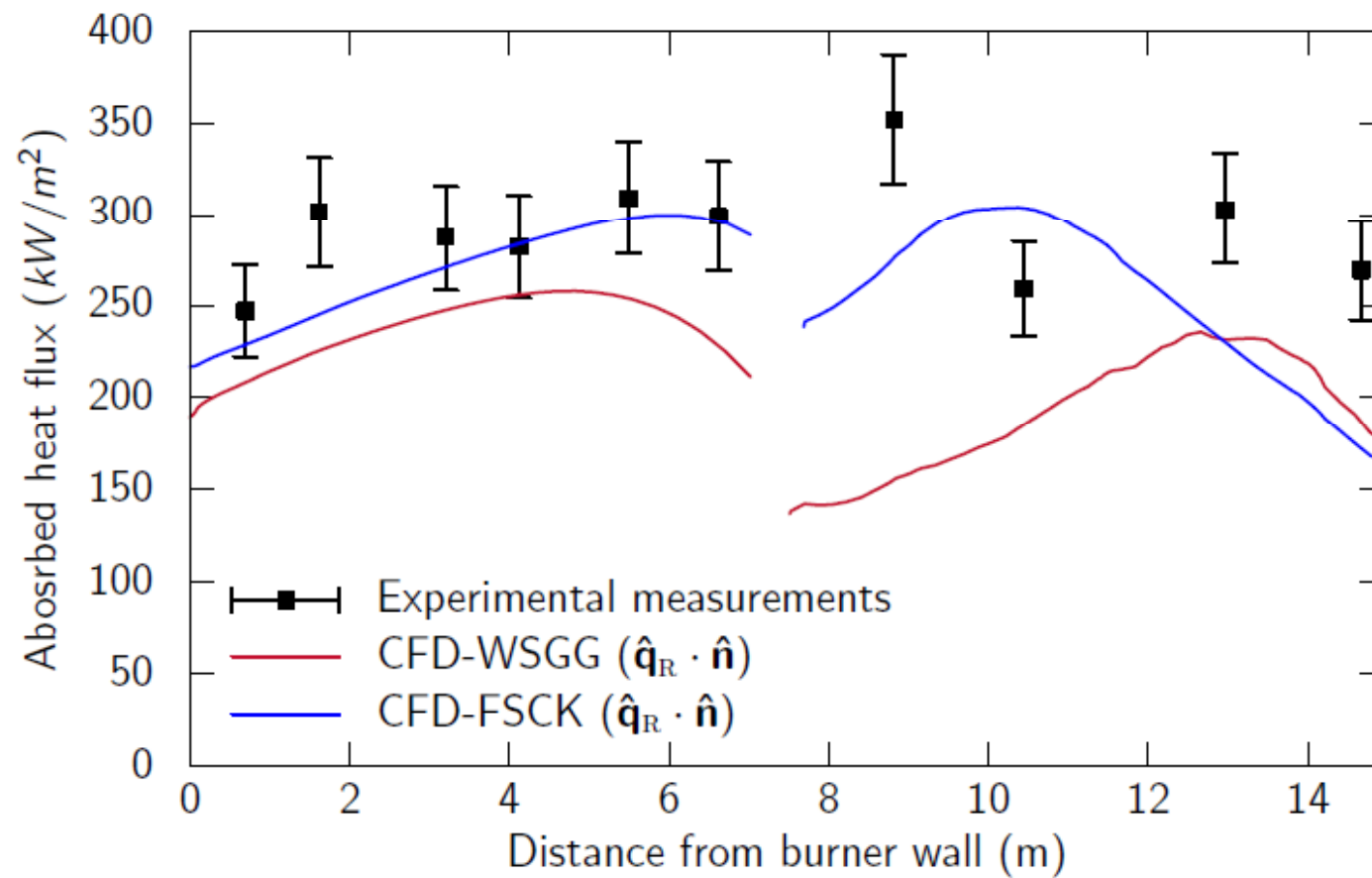
WSGG – Smith et al. (1992)
Y = 0m



FSCK model
Y = 0m

	Exit T.
Measured	1372K
WSGGM	1496K
FSCK	1370K

Results





- Radiation models significantly affect temperature in CFD
- Accurate gas-radiation properties are important for oxyfuel
 - Far higher concentrations of participating gasses
 - Including the FSCK model improves temperature predictions
- Both gas- and particle-phase radiative sources are important
- Further insight required for particle radiation interaction



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- Modest, M. F. and Zhang, H. (2002). The full-spectrum correlated-k distribution for thermal radiation from molecular gas-particulate mixtures. *Journal of Heat Transfer*, 124(1):30-38
- Porter, R., Liu, F., Pourkashanian, M., Williams, A., and Smith, D. (2010). Evaluation of solution methods for radiative heat transfer in gaseous oxy-fuel combustion environments. *Journal of Quantitative Spectroscopy and Radiative Transfer*, 111(14):2084-2094
- Smith, T. F., Shen, Z. F., and Friedman, J. N. (1982). Evaluation of coefficients for the weighted sum of gray gases model. *Journal of Heat Transfer*, 104(4):602-608

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